

# Arsenic adsorption onto lignite under saturated flow conditions: Experiment and reactive transport modeling



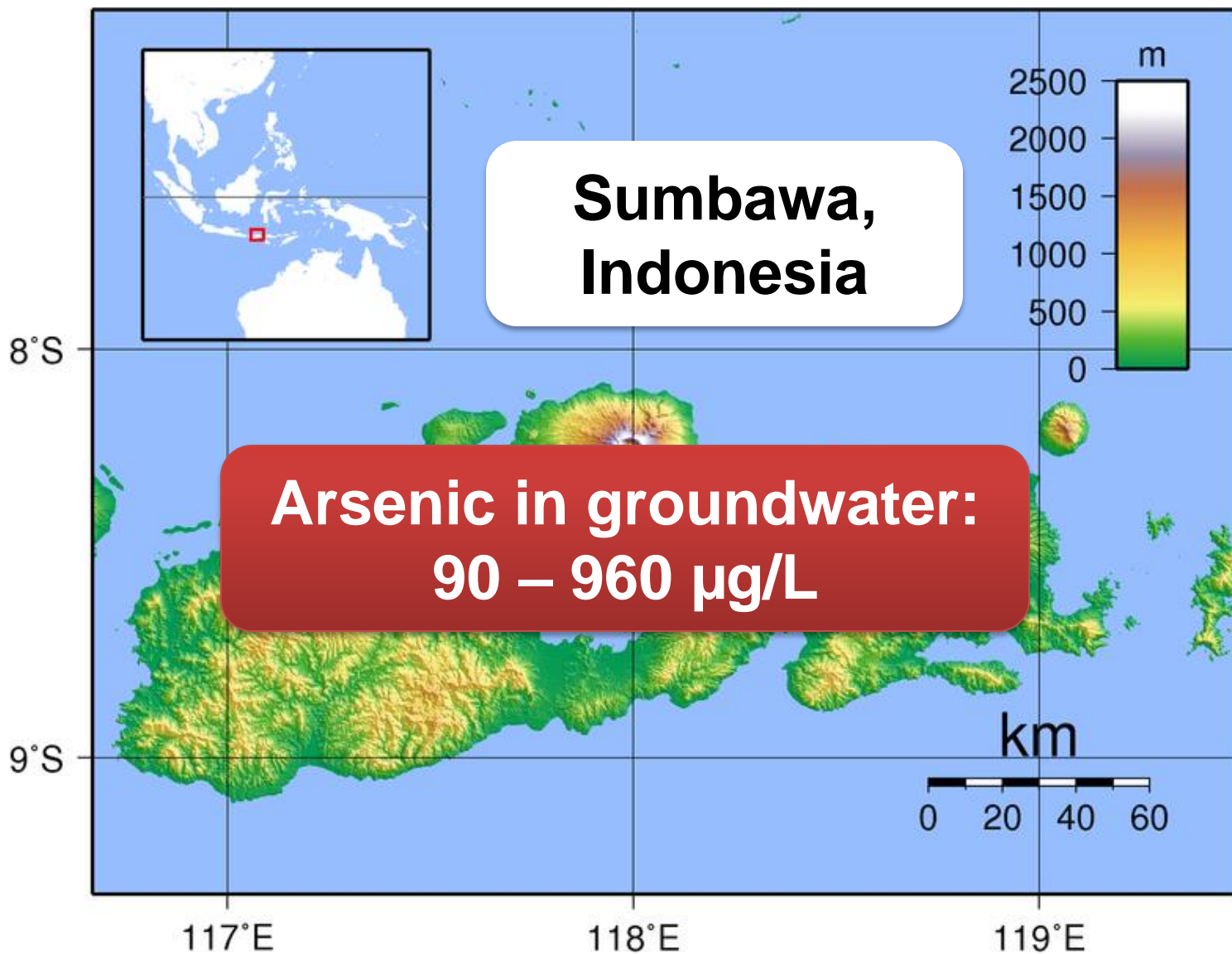
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# What is the motivation in conducting this study?



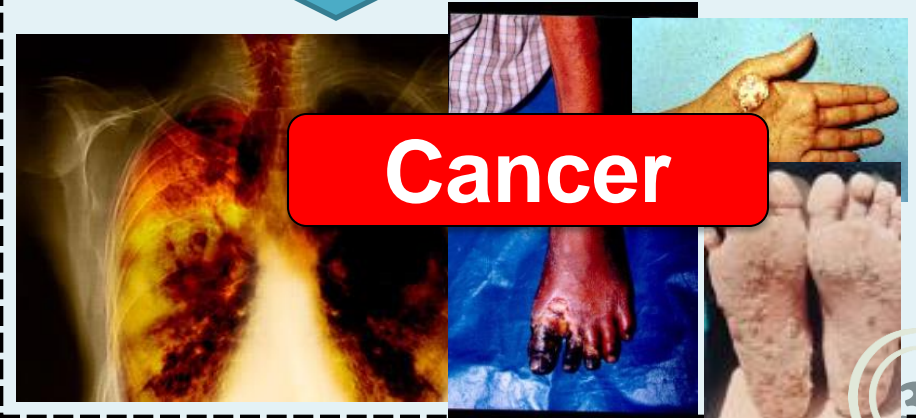
# Why is arsenic problematic?



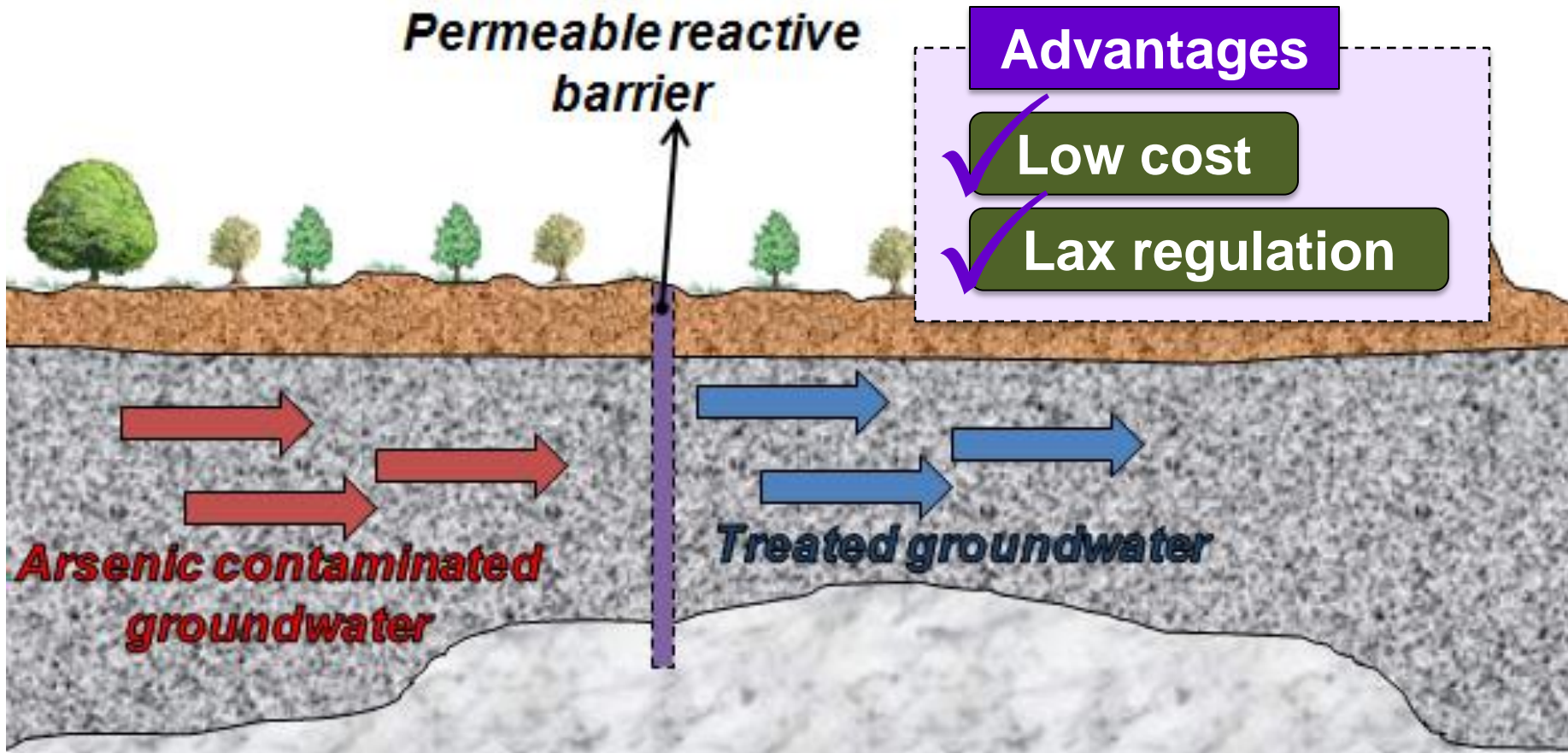
## Acute poisoning



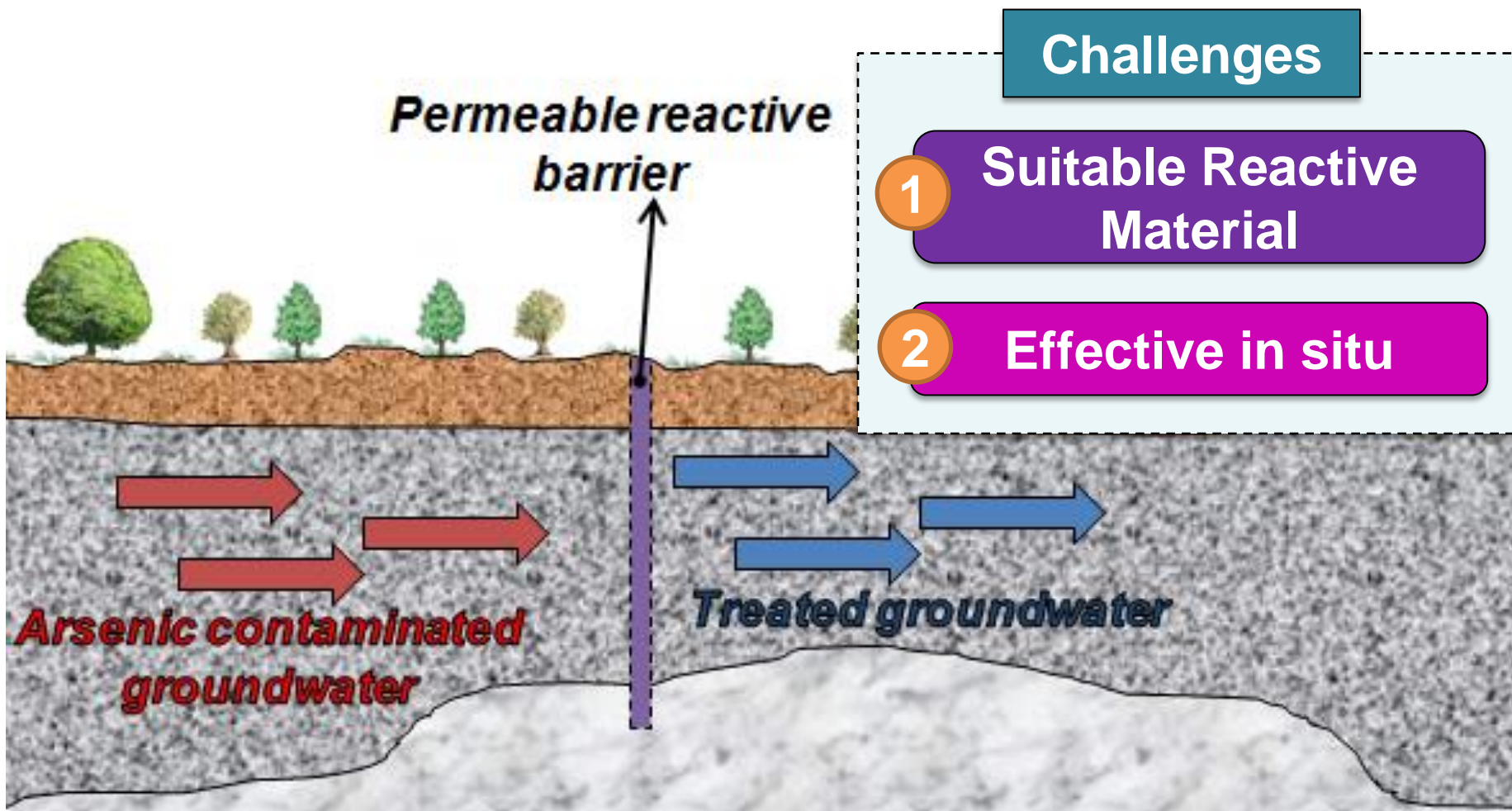
## Chronic poisoning



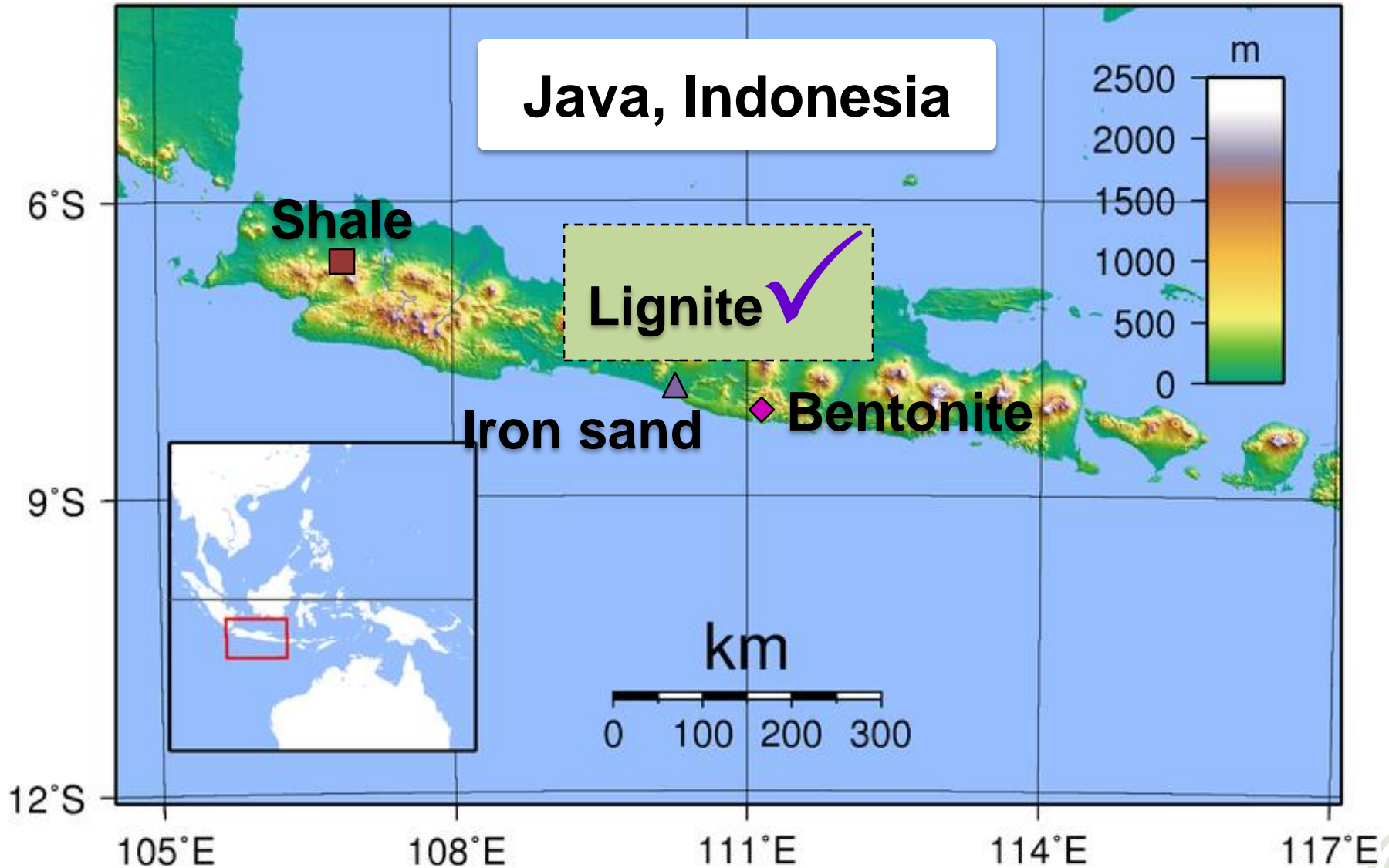
# How can this problem be remediated?



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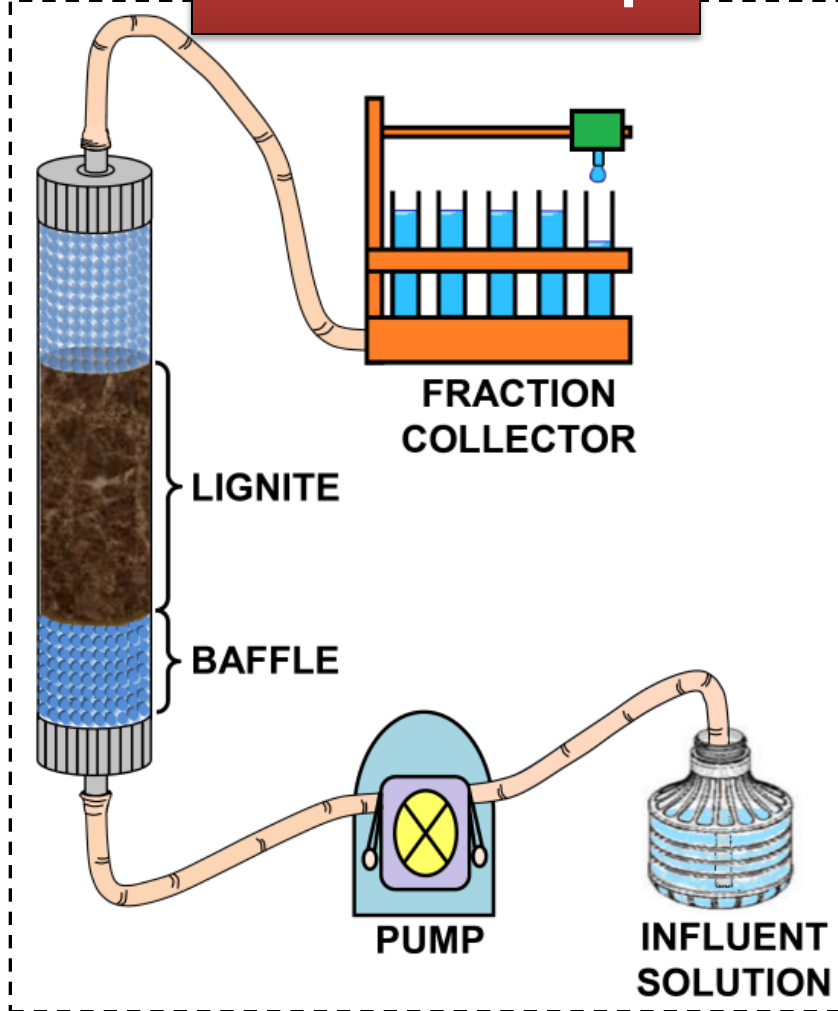
# What potential reactive materials were evaluated?



# What are the objectives of this study?



## Column setup



1

Evaluate the adsorption of arsenic onto lignite under saturated flow conditions

2

Investigate the effects of soluble phases on arsenic adsorption

3

Estimate the  $K_D$  of arsenic onto lignite under saturated flow conditions

# What are the chemical and mineralogical properties of lignite?

Lignite



## Chemical properties

- 💧 Total Organic Carbon = 33 wt.%
- 💧 Arsenic = 1.8 mg/kg

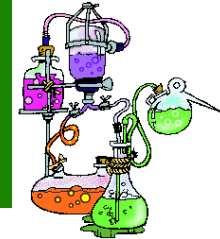
## Mineralogical properties

- 💧 Pyrite ( $\text{FeS}_2$ )
- 💧 Orpiment ( $\text{As}_2\text{S}_3$ )

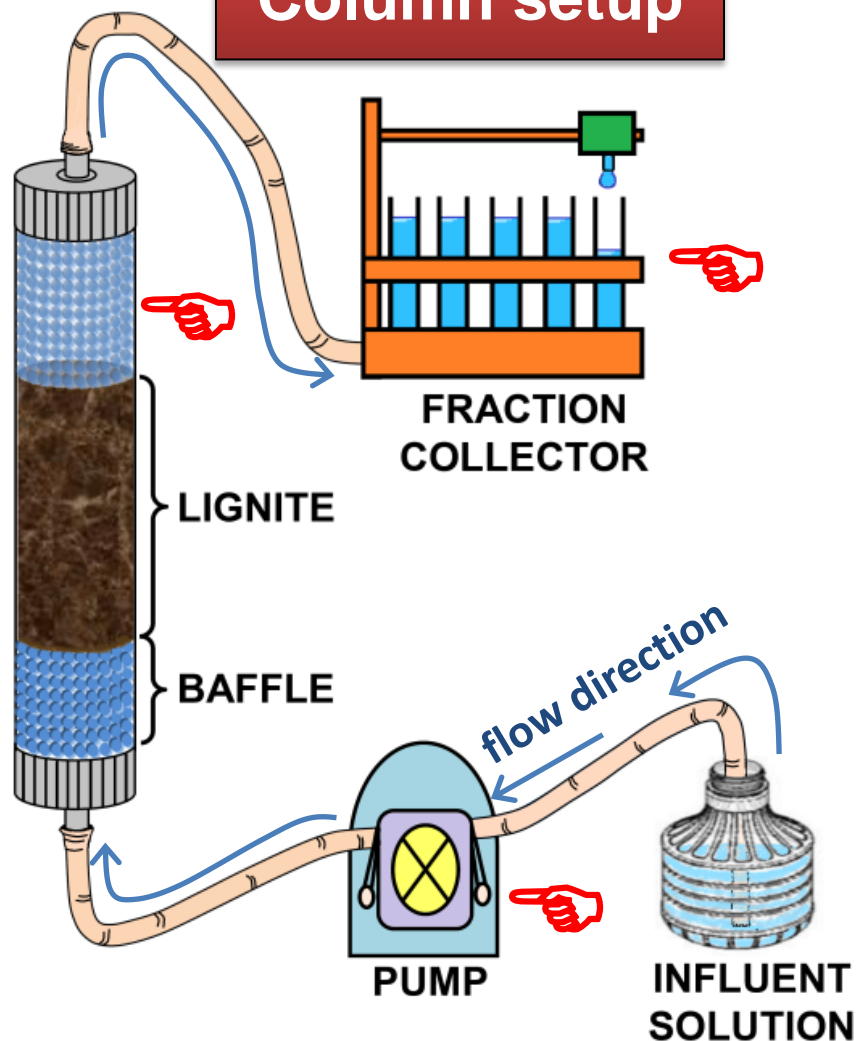
## Leachate properties

- 💧 pH = 2.5 – 2.7
- 💧 Arsenic  $\approx$  0.8  $\mu\text{g/g}$

# Under what conditions were the column experiments conducted?



## Column setup



## Initial and flow conditions

- Weight of adsorbent = 17.35 g
- Thickness = 6 cm
- Particle density = 1.87 g/cm<sup>3</sup>
- Particle size = 0.5 – 1.0 mm
- porosity = 0.658

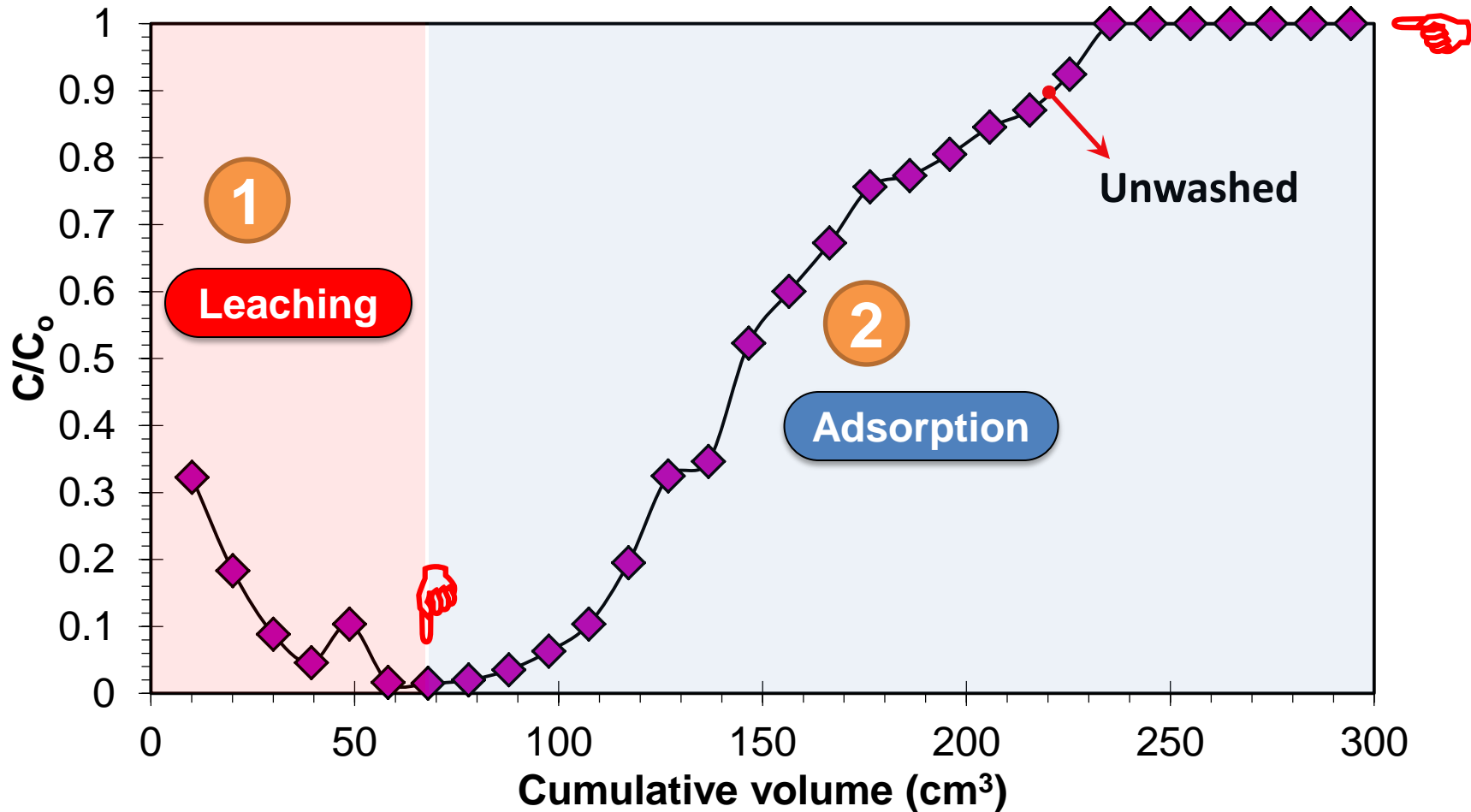
### 1 Unwashed

- Flow rate = 0.224 cm<sup>3</sup>/min
- Lignite was used directly

### 2 Washed

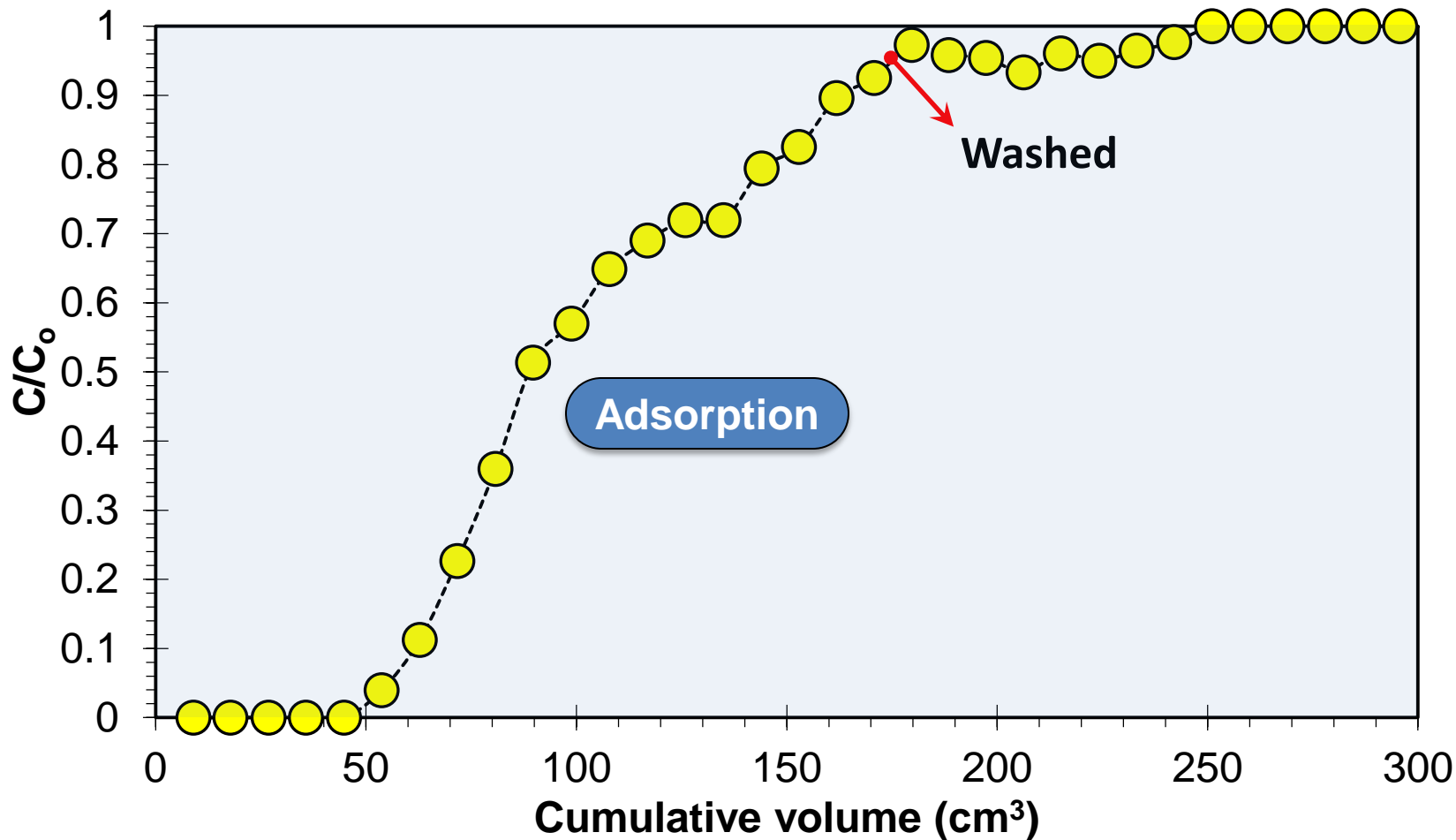
- Flow rate = 0.244 cm<sup>3</sup>/min
- Washed with deionized water for 24 h

# What was the adsorption performance of the unwashed lignite sample?



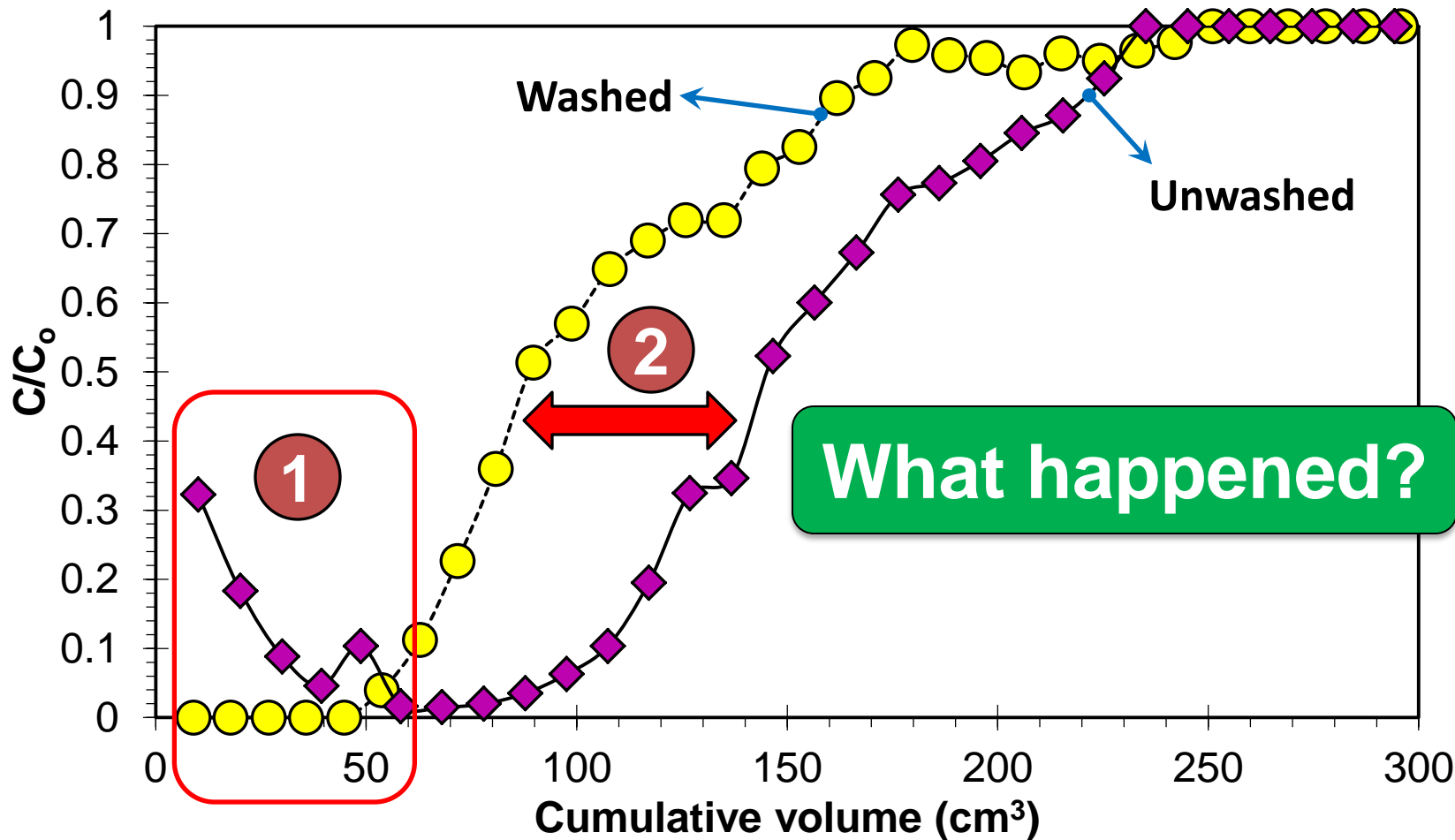
✓The breakthrough curve of arsenic had a leaching and adsorption dominant region.

# What was the adsorption performance of the washed lignite sample?



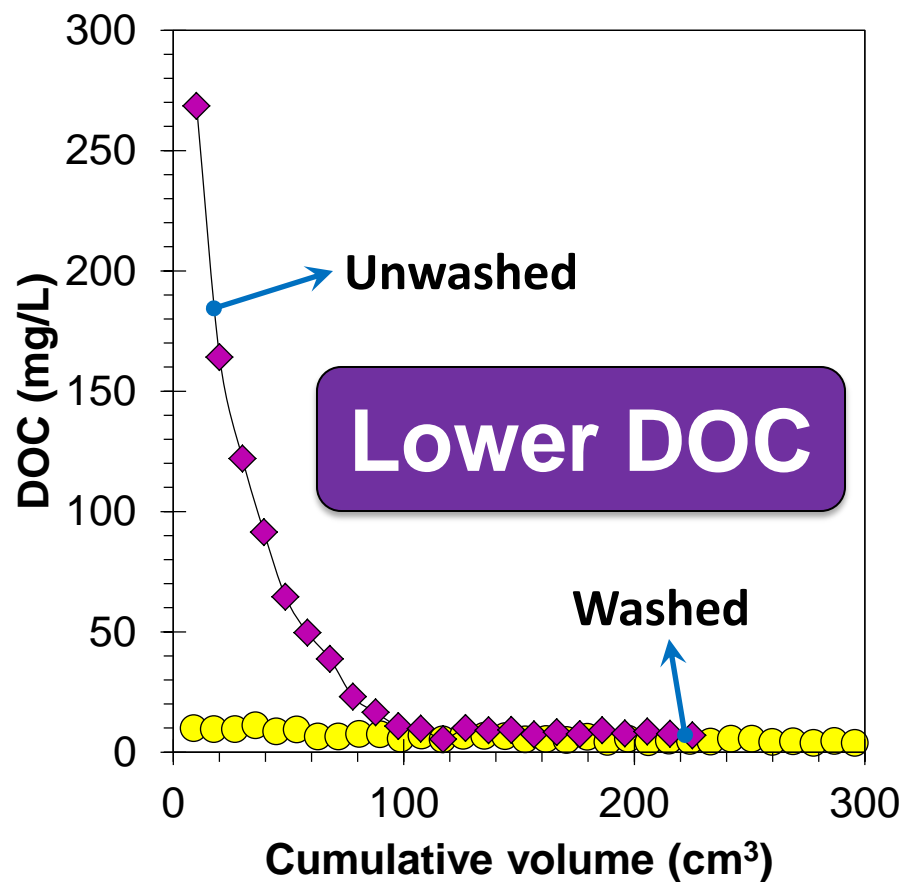
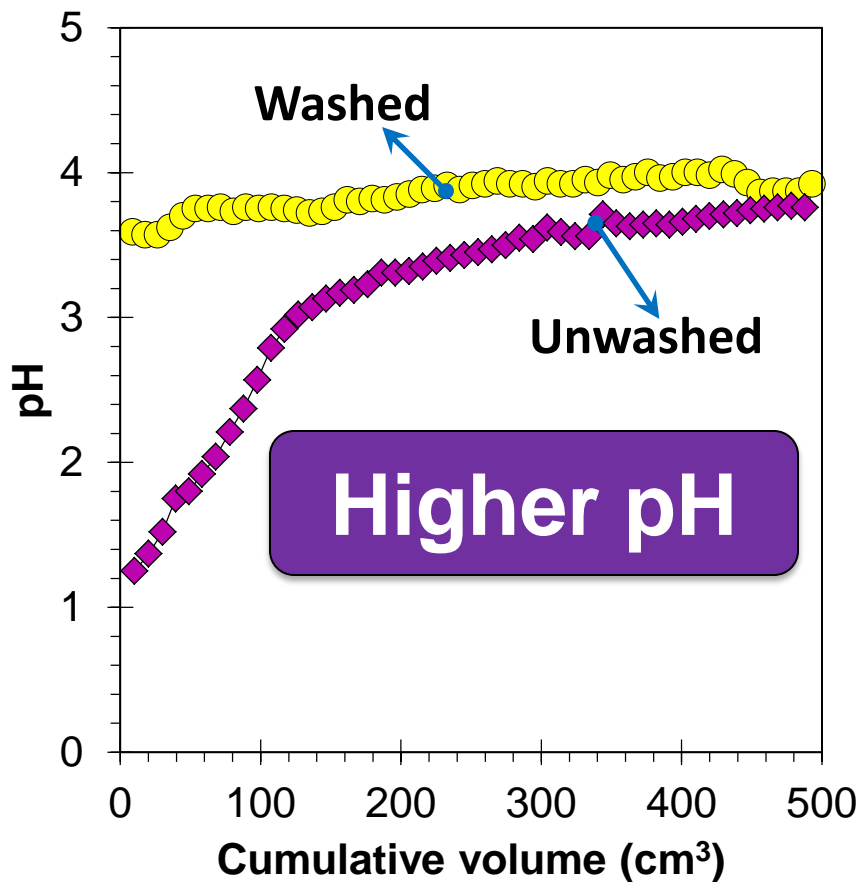
✓The breakthrough curve of arsenic after washing did not contain an initial leaching region.

# What is the adsorption performance of lignite under saturated flow conditions?



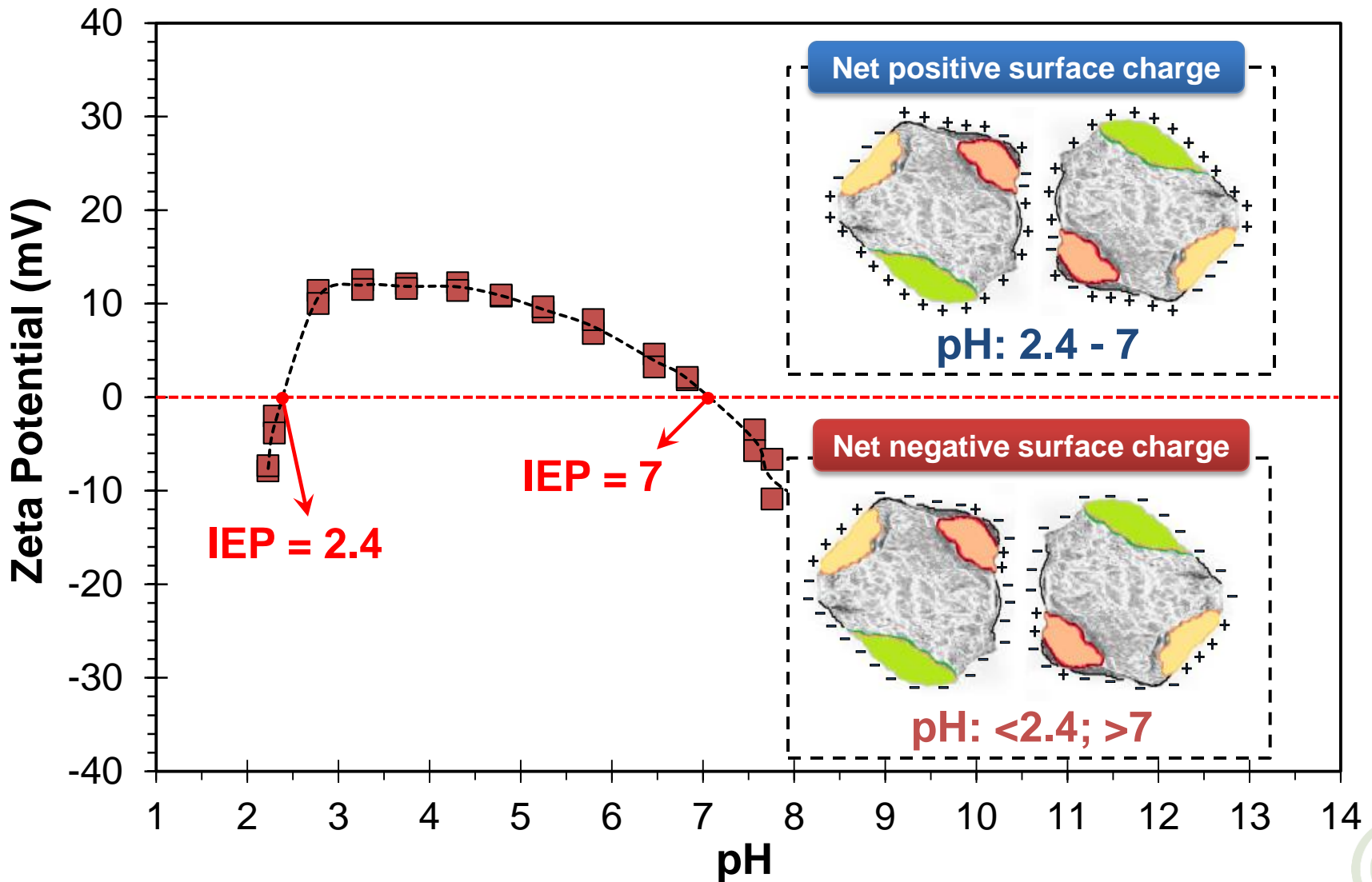
✓ Washing removed the initial leaching region but reduced the overall adsorption capability of lignite.

# Why did the leaching region disappear after washing?

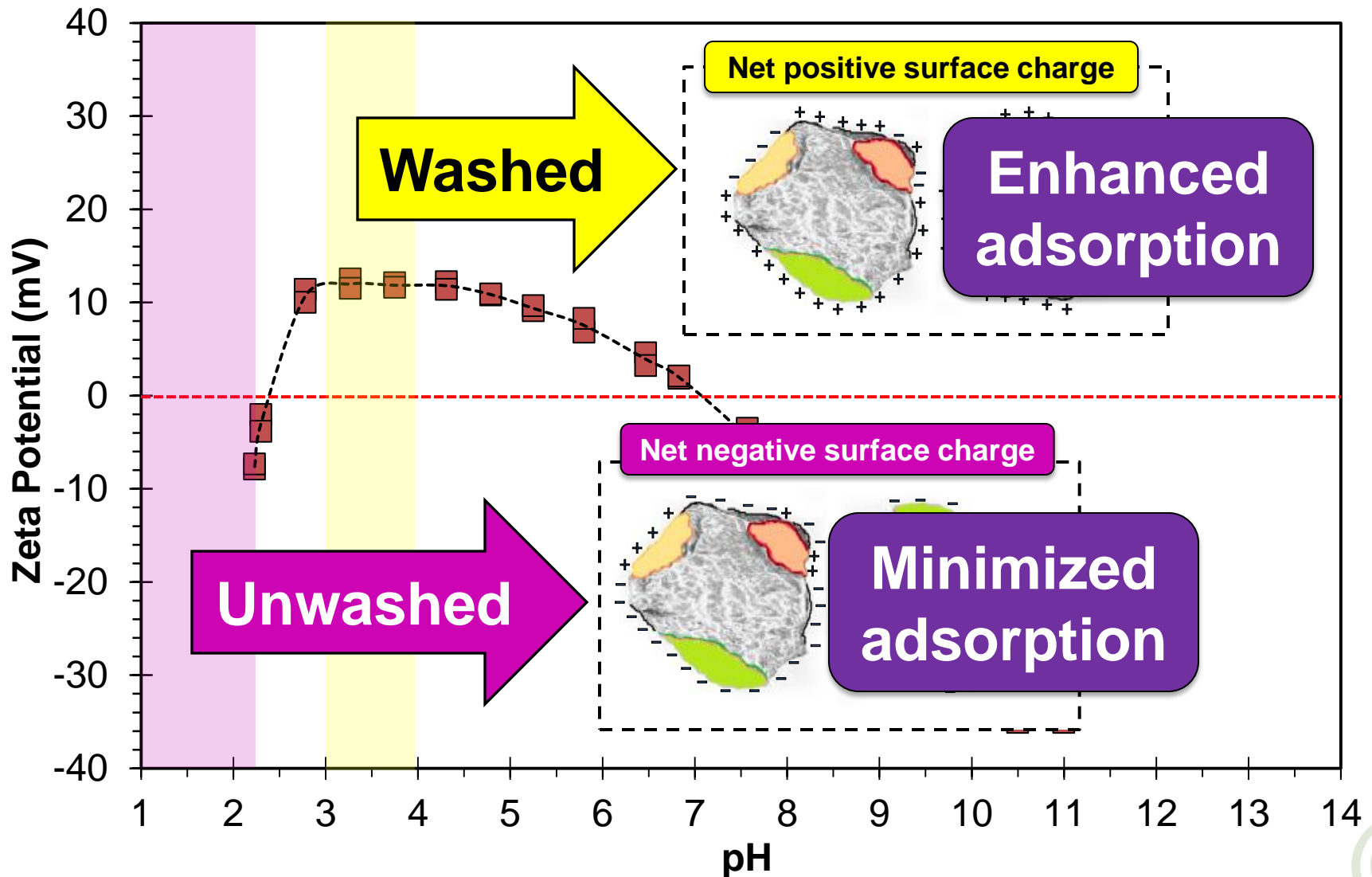


✓ Initially, the effluents from the unwashed sample have very acidic pH and high DOC concentration.

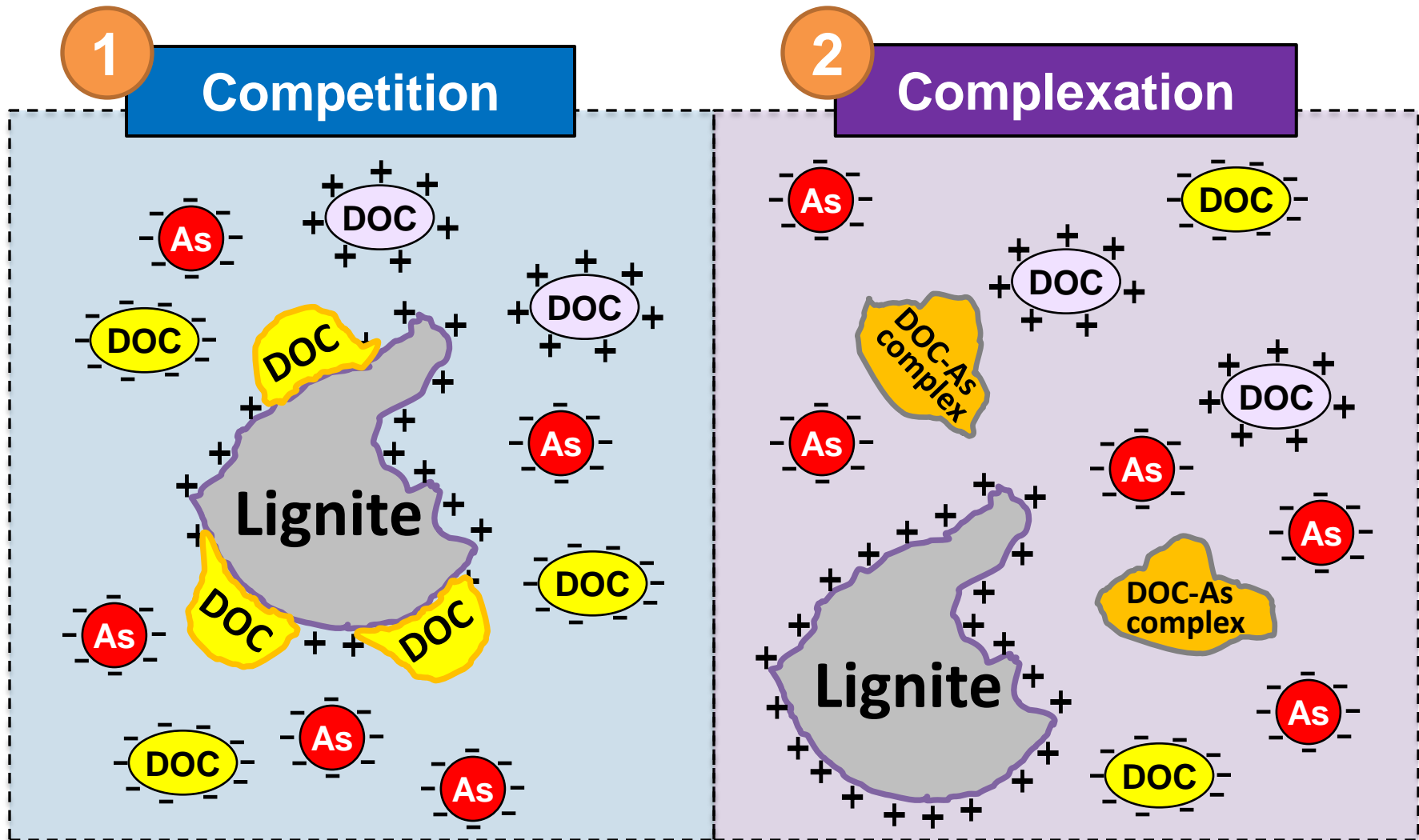
# How did the pH affected arsenic adsorption?



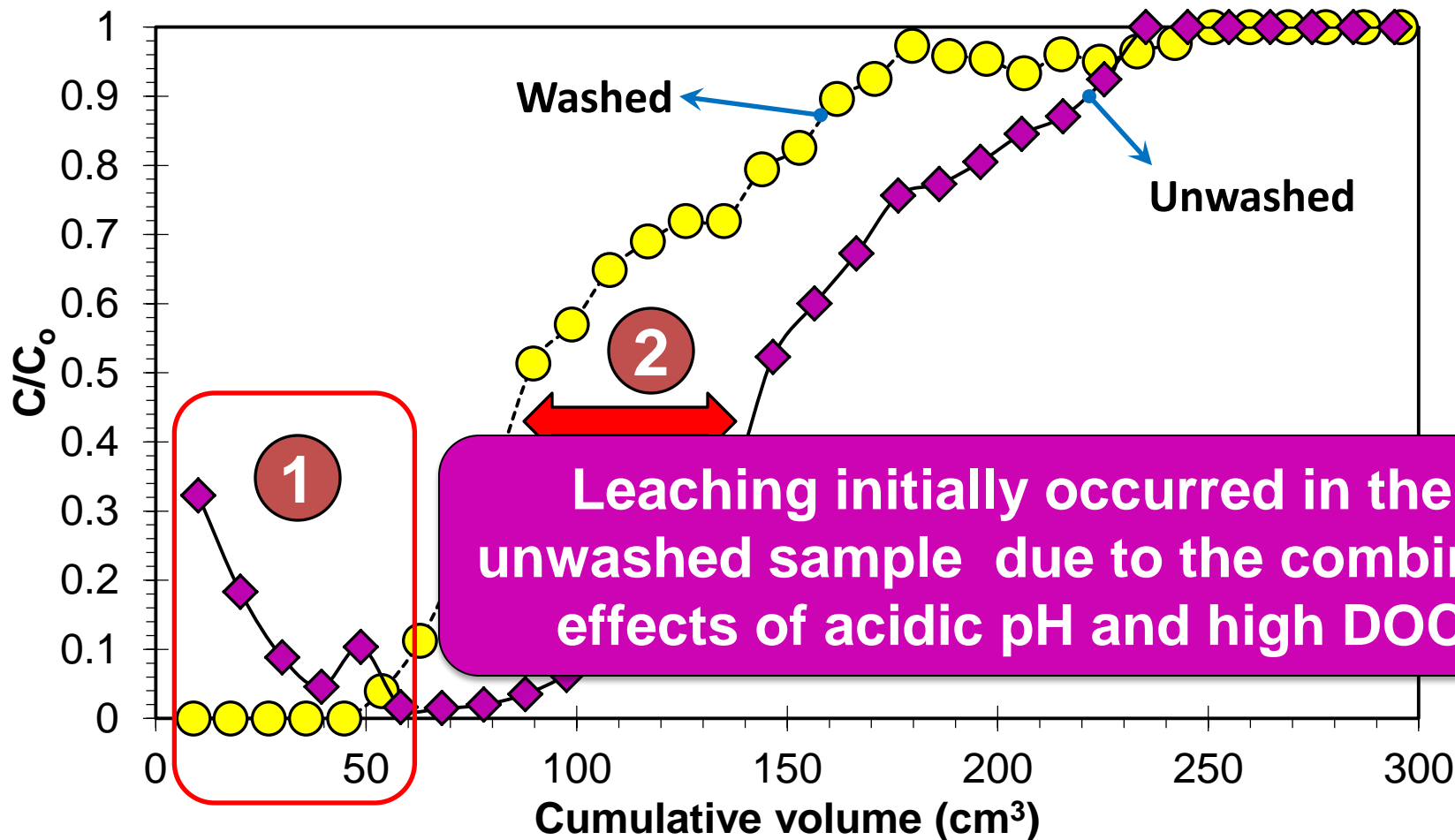
# How did the pH affected arsenic adsorption?



# How did DOC affected arsenic adsorption?

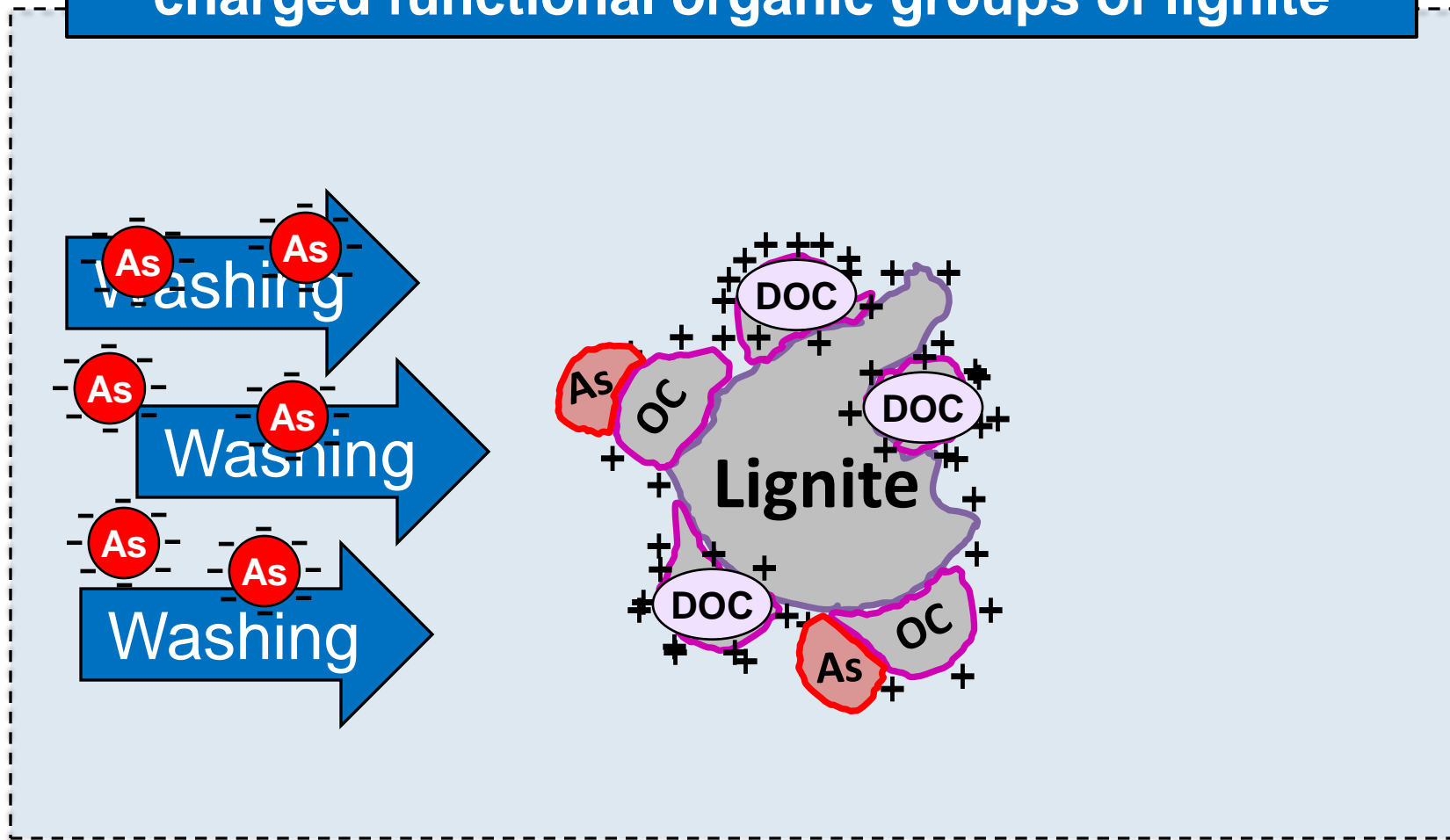


# What is the adsorption performance of lignite under saturated flow conditions?



# Why did the adsorption of arsenic onto lignite decreased after washing ?

Washing removed some of the positively charged functional organic groups of lignite

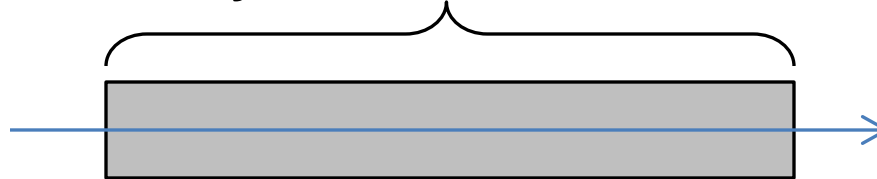


# How was the distribution coefficient ( $K_D$ ) estimated?



## Simulation

1 layer; 6 cm; 100 cells



## Equation

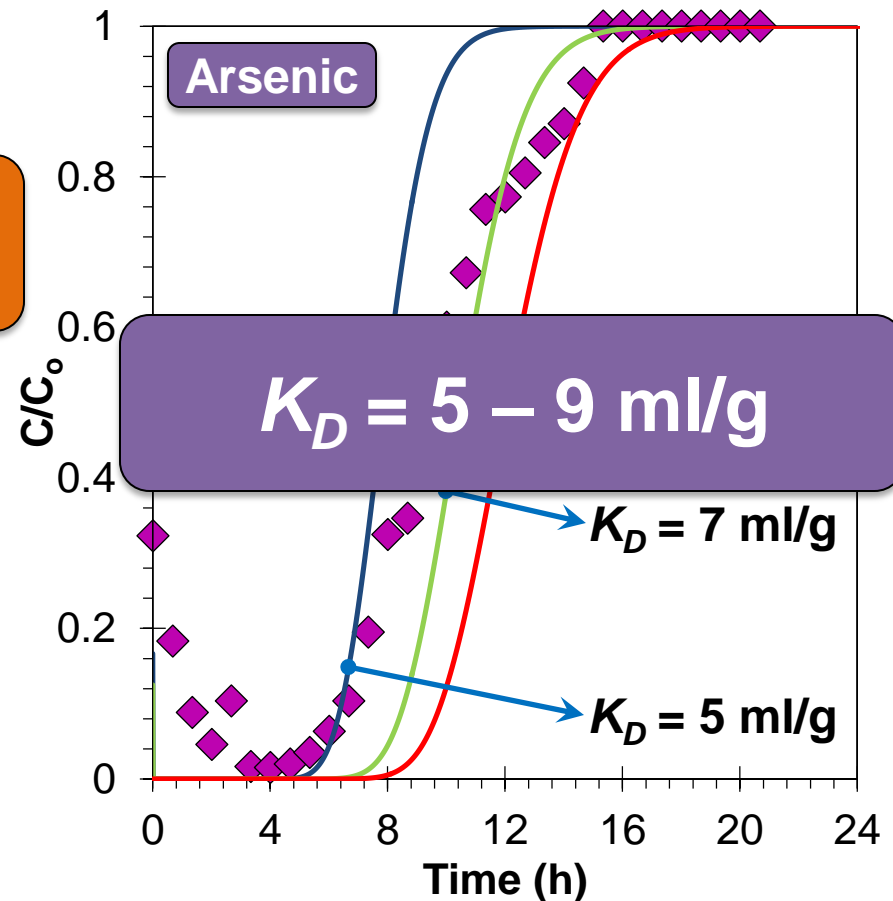
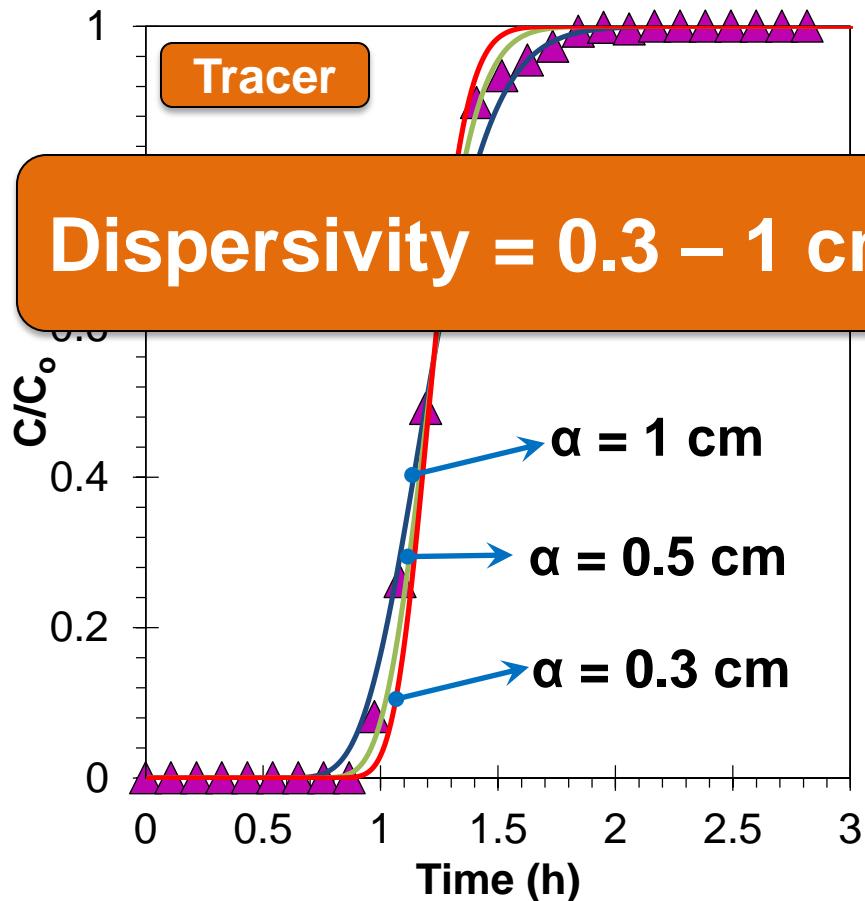
$$D_L \frac{\partial^2 C}{\partial x^2} - \bar{v} \frac{\partial C}{\partial x} - \frac{\partial q}{\partial t} = \frac{\partial C}{\partial t} ; q = K_D * C$$

Dispersion    Advection    Reaction     $\longrightarrow$  Linear adsorption

## Conditions

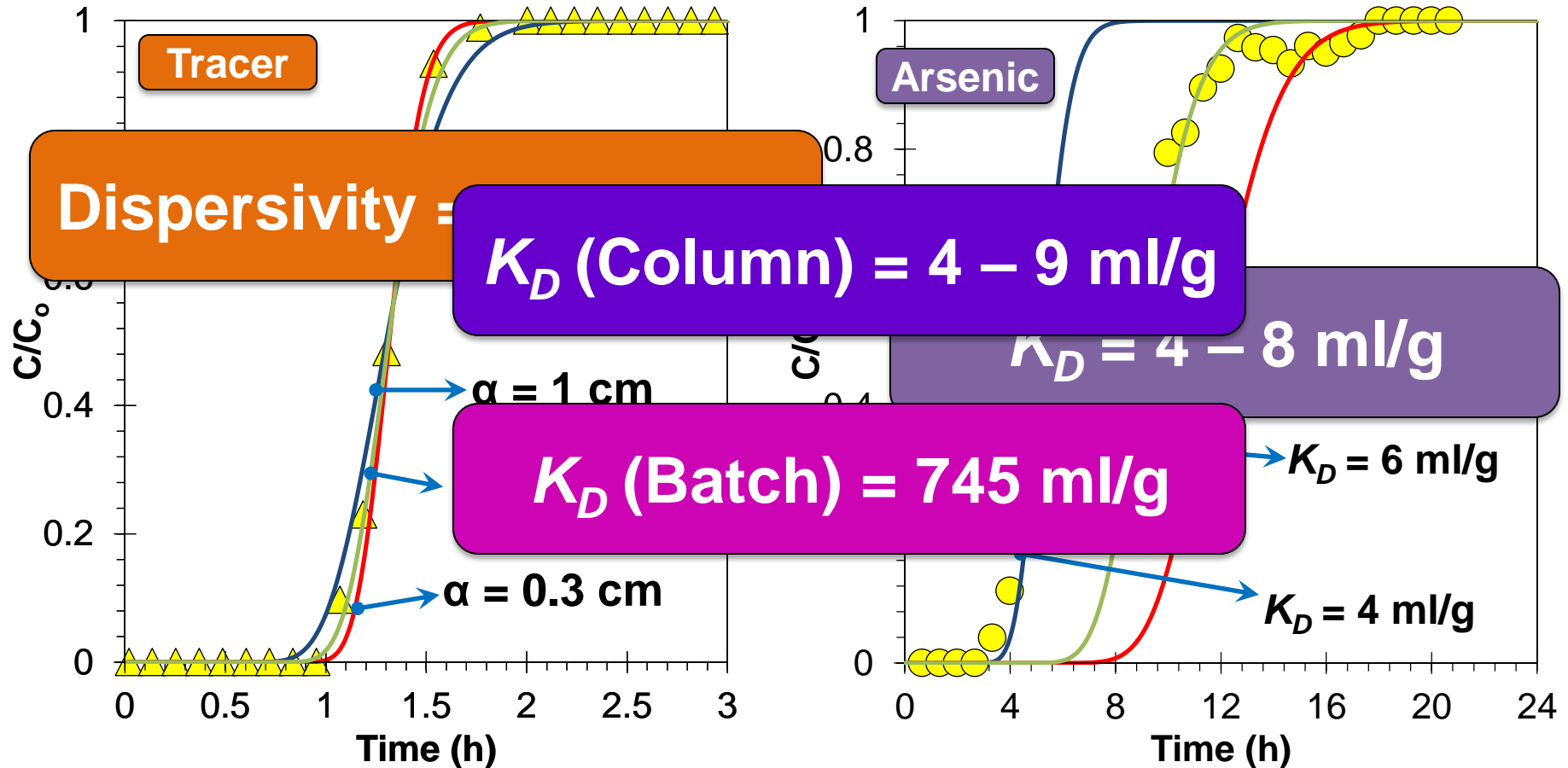
- 💧 Flow condition = Saturated-steady state
- 💧 Flow direction = Forward
- 💧 Solute transport conditions = Flux

# How was the distribution coefficient ( $K_D$ ) estimated?



✓PHREEQC was able to estimate the distribution coefficient of lignite under saturated flow conditions

# How was the distribution coefficient ( $K_D$ ) estimated?



✓ Adsorption of arsenic substantially decreased under saturated flow conditions

# Conclusions



- 💧 Lignite was capable of sequestering arsenic under saturated-steady state flow.
- 💧 The effects of pH and DOC were very pronounced under saturated flow conditions.
- 💧 The one-dimensional advection-dispersion equation with linear adsorption could be used to give rough estimates of the  $K_D$  values of adsorbent materials close to the actual field conditions.

Thank you for listening...



